

Study on the Adsorption Performance of a Direct Air Capture CO₂ Adsorbent

1. Background

Rising atmospheric CO₂ concentrations have intensified interest in carbon-capture technologies capable of achieving negative emissions. Among these, Direct Air Capture (DAC) removes CO₂ directly from ambient air, where the partial pressure of CO₂ is approximately 40 Pa, far lower than flue gas concentrations (~12 kPa). This low driving force imposes stringent requirements on adsorbent materials and limits the applicability of membrane separation or cryogenic methods. Solid sorbents, in contrast to liquid amine solutions, avoid issues associated with solvent volatility, corrosion, and high regeneration energy, making them well-suited for DAC systems.⁽¹⁾

A wide range of solid sorbents has been explored, including alkali/alkaline-earth materials, metal-organic frameworks (MOFs), supported amines, and hybrid wet adsorbents.⁽²⁾ Effective DAC sorbents must combine high CO₂ adsorption capacity, rapid kinetics, and strong CO₂/N₂ and CO₂/H₂O selectivity, while also maintaining stability across multiple adsorption-desorption cycles. Literature studies illustrate the challenges and potential approaches. For example, amine-grafted porous polymer networks (PPNs) demonstrate high selectivity at 400 ppm CO₂, and microporous MOFs modified with silica-rich additives exhibit substantial improvements in CO₂ uptake due to enhanced micropore volume.^(3,4) Other works highlight the significant influence of humidity, as water molecules may compete with CO₂ for adsorption sites on hydrophilic surfaces, reducing CO₂ selectivity and breakthrough performance.⁽⁵⁾

In this study, we investigate the pore-structure characteristics and CO₂ adsorption performance of a MOF adsorbent using N₂ physisorption, CO₂ physisorption, TGA-based adsorption measurements, and CO₂ breakthrough experiments with the goal of understanding how surface area, pore structure, and ambient humidity influence DAC-relevant performance metrics. These measurements provide a foundation for evaluating the suitability of the material for DAC applications and for optimizing future sorbent designs.

2. Experiment

A MOF-based adsorbent was selected for characterization under DAC-relevant conditions, including N₂ physisorption, CO₂ adsorption isotherms, TGA adsorption capacity testing, and breakthrough curve analysis.

Nitrogen adsorption-desorption isotherms were measured at 77 K using a **Matrix 1000** specific surface area and pore size analyzer from **AMI**. The data was used to calculate the BET surface area, micropore volume, and pore size distribution.

CO₂ adsorption isotherms at 25 °C were also measured using the **Matrix 1000** analyzer from **AMI**.

The **TGA 1000** thermogravimetric analyzer from **AMI** was used to determine CO₂ uptake under two conditions:

- ✓ Pure CO₂, 50 mL/min, pretreatment at 80 °C followed by adsorption at 25 °C
- ✓ 400 ppm CO₂ / N₂ mixture, 50 mL/min carrier gas, with pretreatment and adsorption performed at 80 °C and 25 °C respectively.

Breakthrough tests were performed using a **BTsorb 100** penetration curve and mass-transfer analyzer from **AMI** at 400 ppm CO₂, 40% relative humidity, 10 mL/min flow, 298 K, and 1 bar. Breakthrough profiles were used to calculate dynamic adsorption capacity under humid DAC conditions.

3. Results

As shown in Figure 1a, the MOF material exhibits a Type I isotherm, characteristic of a microporous adsorbent. The BET surface area was measured as 1160 m²/g, with a micropore volume of 0.438 cm³/g and a maximum pore width of 0.390 nm, indicating an abundance of ultramicropores well-suited for CO₂ adsorption at low pressures.

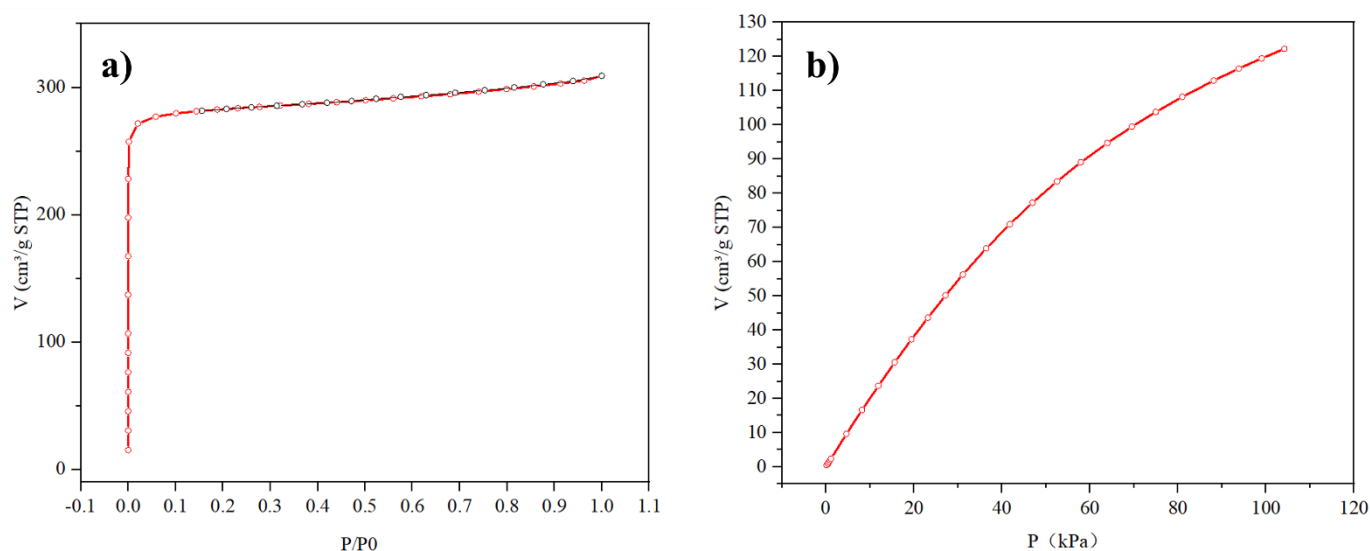


Figure 1: a) N₂ adsorption and desorption isotherms at 77 K and b) CO₂ adsorption isotherms at 298 K obtained using the **Matrix 1000**

At 298 K and 1 bar, the CO₂ saturated adsorption capacity, shown in Figure 1b, reached 119 cm³/g (5.431 mmol/g), reflecting strong interaction between CO₂ molecules and the microporous network. This high capacity is consistent with the MOF material's large surface area and concentration of narrow micropores, which enhance adsorption potential energy in low-pressure regimes.

TGA measurements under pure CO₂ (Figure 2a) showed an uptake of 4.42 mmol/g, in agreement with the volumetric isotherm data. Under dilute CO₂ conditions (400 ppm), the measured capacity was 0.13 mmol/g (Figure 2b), substantially lower than the pure-gas capacity. This reduction is expected

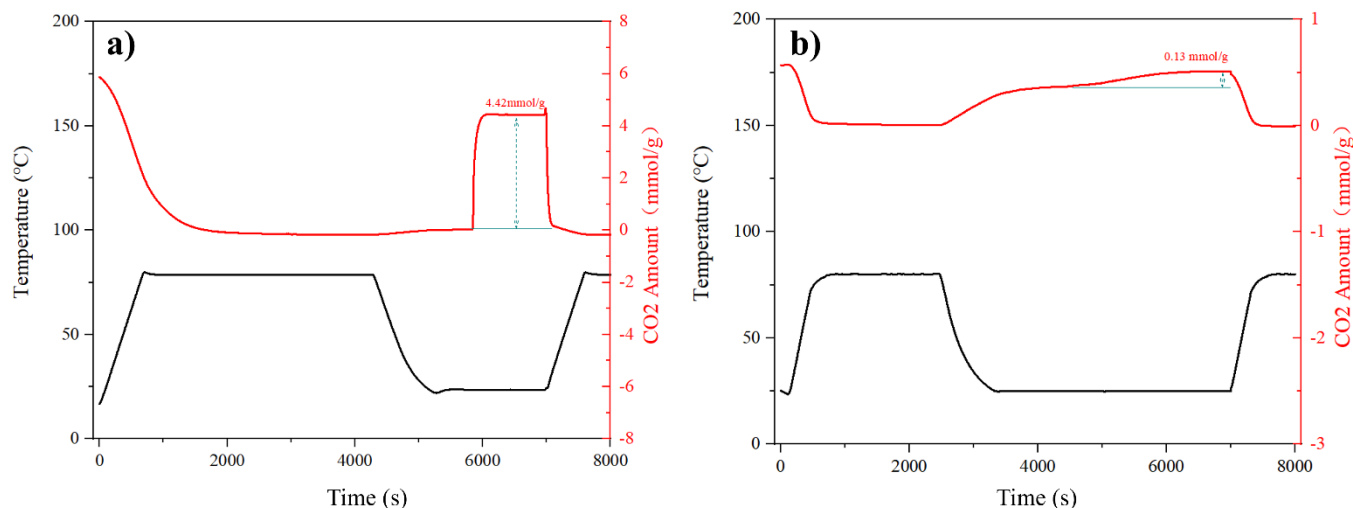


Figure 2: a) Pure CO₂ adsorption capacity and b) 400 ppm CO₂ adsorption capacity under dry conditions, determined by TGA experiments with the **TGA 1000**

because low CO₂ partial pressure decreases the frequency of CO₂–surface collisions and reduces the probability of pore filling, especially in ultramicropores where adsorption is strongly pressure-dependent.

Breakthrough testing at 40% relative humidity (Figure 3) resulted in a dynamic CO₂ capacity of 0.004 mmol/g, significantly lower than under dry conditions. The presence of water vapor likely introduces competitive adsorption on hydrophilic sites, reducing CO₂ selectivity, particularly at low concentrations typical of DAC applications. This observation underscores the importance of hydrophobic surface modification or tailored pore environments for adsorbents intended for humid-air CO₂ capture.

4. Conclusions

This study demonstrates that the MOF adsorbent possesses a high specific surface area and well-defined micropore structure, enabling substantial CO₂ adsorption under idealized, dry conditions. However, performance decreases sharply at low CO₂ partial pressures and in the presence of humidity, primarily due to competitive adsorption and reduced collision frequency. These findings highlight the need for surface hydrophobization, amine functionalization, or pore-environment tuning to improve DAC applicability.

From a measurement standpoint, the combined use of N₂ physisorption, volumetric CO₂ isotherms, and TGA adsorption analysis provides a comprehensive understanding of sorbent performance. The **Matrix 1000**, **TGA 1000**, and **BTsorb 100** all offer high sensitivity measurements for low-pressure

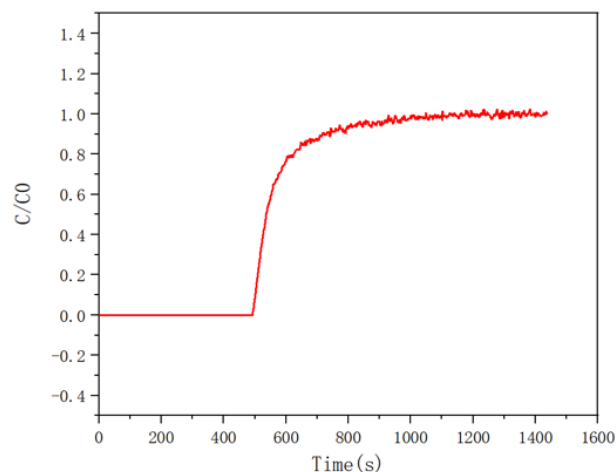


Figure 3: 400 ppm CO₂ penetration curve of a sample at 40% humidity, obtained with the **BTsorb 100**

adsorption, precise temperature control, and robust repeatability—critical for evaluating DAC sorbents where small differences in uptake are scientifically meaningful.

5. References

- (1) McQueen, N.; Gomes, K. V.; McCormick, C.; Blumanthal, K.; Pisciotta, M.; Wilcox, J. A review of direct air capture (DAC): Scaling up commercial technologies and innovating for the future. *Prog. Energy*, **2021**, *3*, 032001.
- (2) Chuah, C. Y.; Ho, Y. L.; Syed, A. M. H.; Thivyalakshmi, K. G. K.; Yang, E.; Johari, K.; Yang, Y.; Poon, W. C. Applicability of adsorbents in direct air capture (DAC): Recent progress and future perspectives. *Ind. Eng. Chem. Res.* **2025**, *64*, 4117-4147.
- (3) Bose, S.; Sengupta, D.; Rayder, T. M.; Wang, X.; Kirlikovali, K. O.; Sekizkardes, A. K.; Islamoglu, T.; Farha, O. K. Challenges and opportunities: Metal-organic frameworks for direct air capture. *Adv. Funct. Mater.* **2024**, *34*, 2307478.
- (4) Sekizkardes, A. K.; Wang, P.; Hoffman, J.; Budhathoki, S.; Hopkinson, D. Amine-functionalized porous organic polymers for carbon dioxide capture. *Mater. Adv.* **2022**, *3*, 6668.
- (5) Bayati, B.; Keshavarz, F.; Rezaei, N.; Zendejboudi, S.; Barbiellini, B. New insight into impact of humidity on direct air capture performance by SIFSIX-3-Cu MOF. *Phys. Chem. Chem. Phys.* **2024**, *26*, 17645-17659.